

Modeling of Fluid Flow and Heat Transfer During a Steam-Thermolysis Process for Recycling Carbon Fiber Reinforced Polymer

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Introduction

Different types of technologies to recycle carbon fiber reinforced polymer (CFRP) waste have been studied. The steam-thermolysis is a process that combines pyrolysis and superheated steam at atmospheric pressure to decompose the organic matrix of the composite. The waste is introduced into a bench-scale reactor heated at high temperatures under nitrogen atmosphere. A humidity generator is coupled in the reactor gas inlets to provide a flux of superheated steam. A 3D model was built using COMSOL Multiphysics Software to better understand velocity and temperature profiles during the steam-thermolysis process within the reactor.

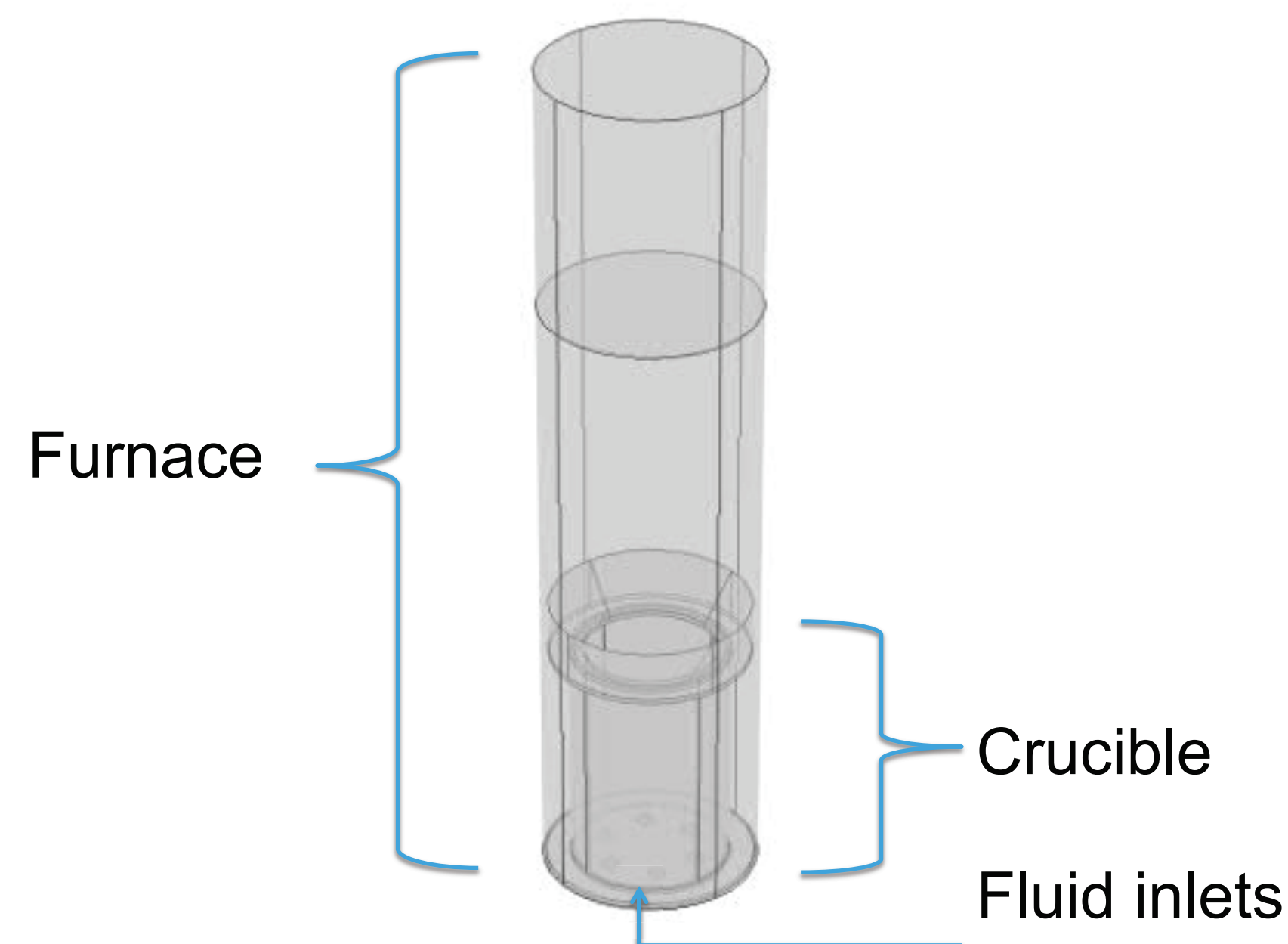


Figure 1. 3D reactor geometry

Computational Methods:

Fluid flow

The hypothesis on the flow regime was justified by calculating Reynolds number with the maximum steam flow rate used during the steam-thermolysis.

$$Re = \frac{\rho \times v \times 2r}{\mu} = 13 < 2000 \quad * \quad (\text{Régime laminaire})$$

The Navier-Stokes equations were applied to model the fluid flow within the furnace.

$$\rho(\mathbf{u} \cdot \nabla)\mathbf{u} = \nabla \cdot \left[-P + \mu(\nabla\mathbf{u} + (\nabla\mathbf{u})^T) - \frac{2}{3}\mu(\nabla \cdot \mathbf{u}) \right] + \mathbf{F} \quad *$$

$$\nabla \cdot (\rho\mathbf{u}) = 0 \quad (\text{compressible flow})$$

Boundary conditions

Inlet: steam flow rate $W_m = 50 - 200 \text{ g/h}$;
 Outlet: $P = 1 \text{ atm}$;
 Wall: no slip ($\mathbf{u} = 0$).

Heat Transfer

A general heat transfer equation including conduction, convection and radiation was used in the model.

$$\rho C_p \mathbf{u} \cdot \nabla T = \nabla \cdot (k \nabla T) + Q \quad *$$

Surface to surface radiation interface was also applied to simulate the radiation effect.

$$J = (1 - \varepsilon)G + \varepsilon\sigma T^4 \quad *$$

Boundary conditions

Inlet: $T_e = 400-500^\circ\text{C}$;
 Outlet: $-\mathbf{n} \cdot (-k \nabla T) = 0$;
 Furnace temperature: $T = T_e + 100^\circ\text{C}$;
 Heat source (Q): Heat released from the reaction.

*p: the density of fluid kg m^{-3} ; u: the velocity m s^{-1} ;
 μ: the dynamic viscosity Pa s ; P: pressure Pa ;
 F: the vector of volume forces N m^{-3} ; Cp: the specific heat capacity of the fluid $\text{kJ kg}^{-1}\text{K}^{-1}$; T: temperature K ;
 k: thermal conductivity of the materials $\text{W m}^{-1}\text{K}^{-1}$;
 Q: heat source W m^{-3}

Results

Without composite

The fluid velocity is more sensitive to steam flow rate changes than temperature changes;

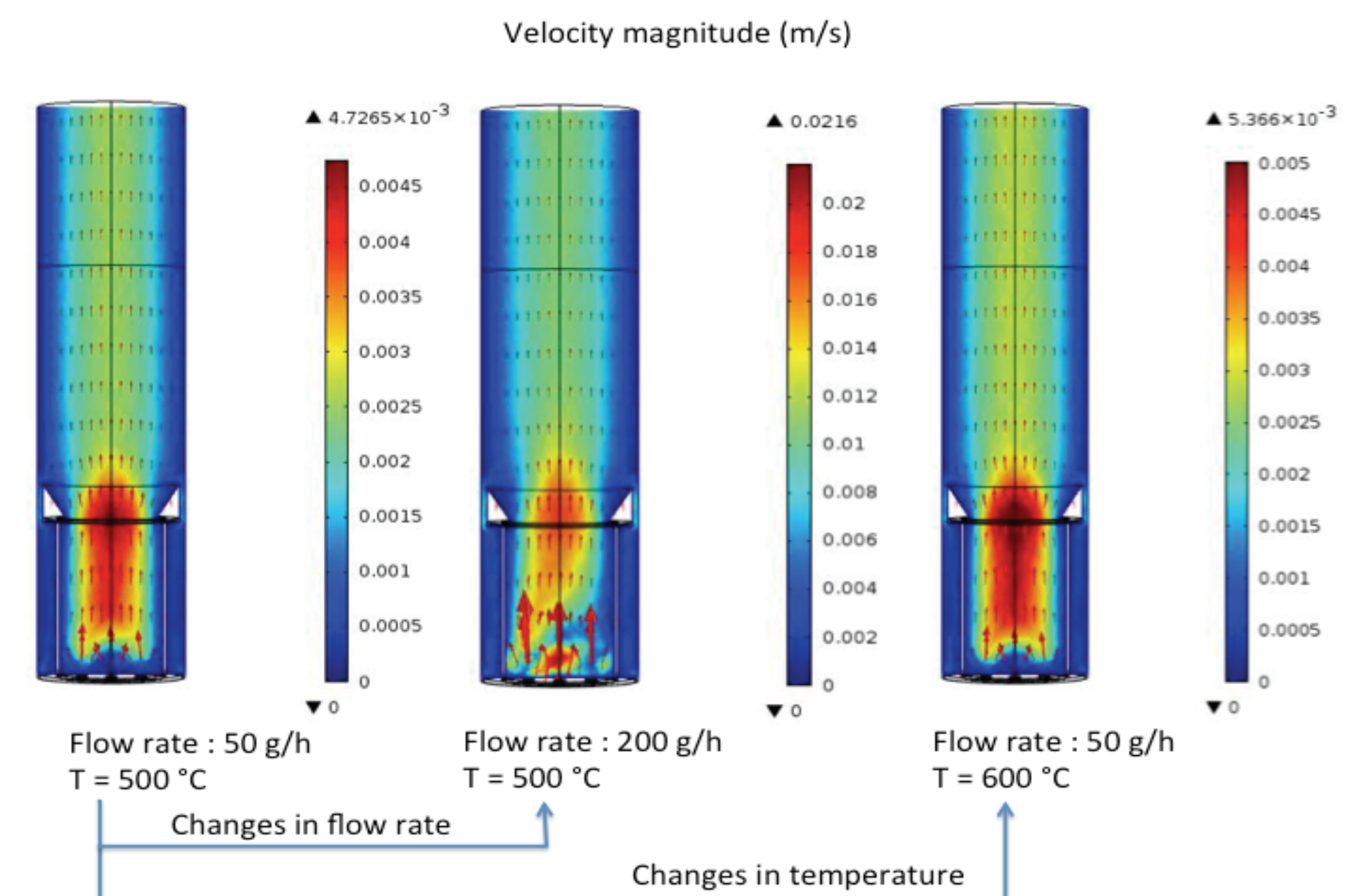


Figure 2. Effects of different parameters on velocity profile

The temperature decreased when the flow rate increases.

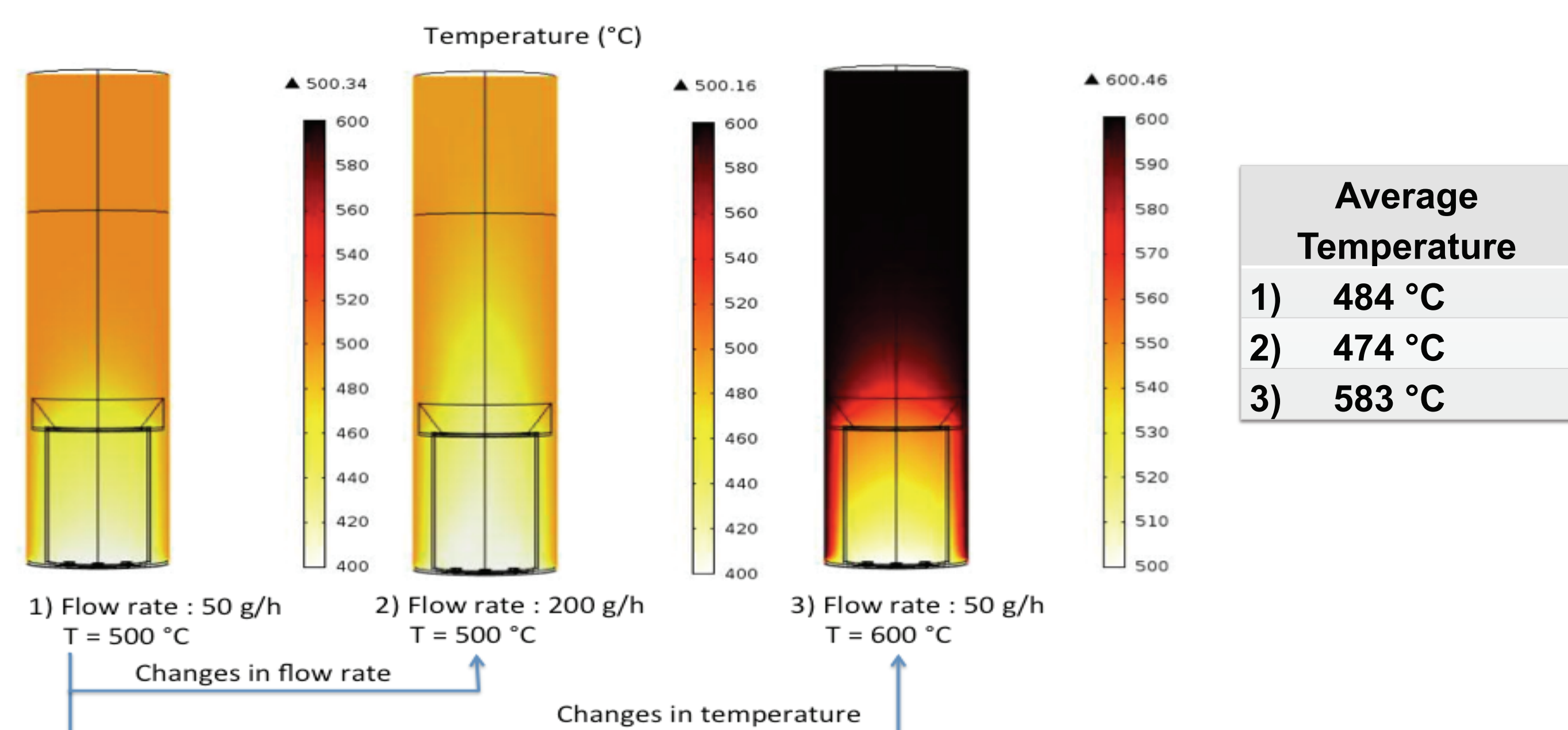


Figure 3. Effects of different parameters on temperature profile

Composite influence

- The introduction of composites produces an increase of the fluid velocity at crucible inlet;
- The environment around the composite becomes colder when the number of composites pieces increases.

Piece in the center Piece in the corner Several pieces (=60)

Figure 4. Pieces arrangements

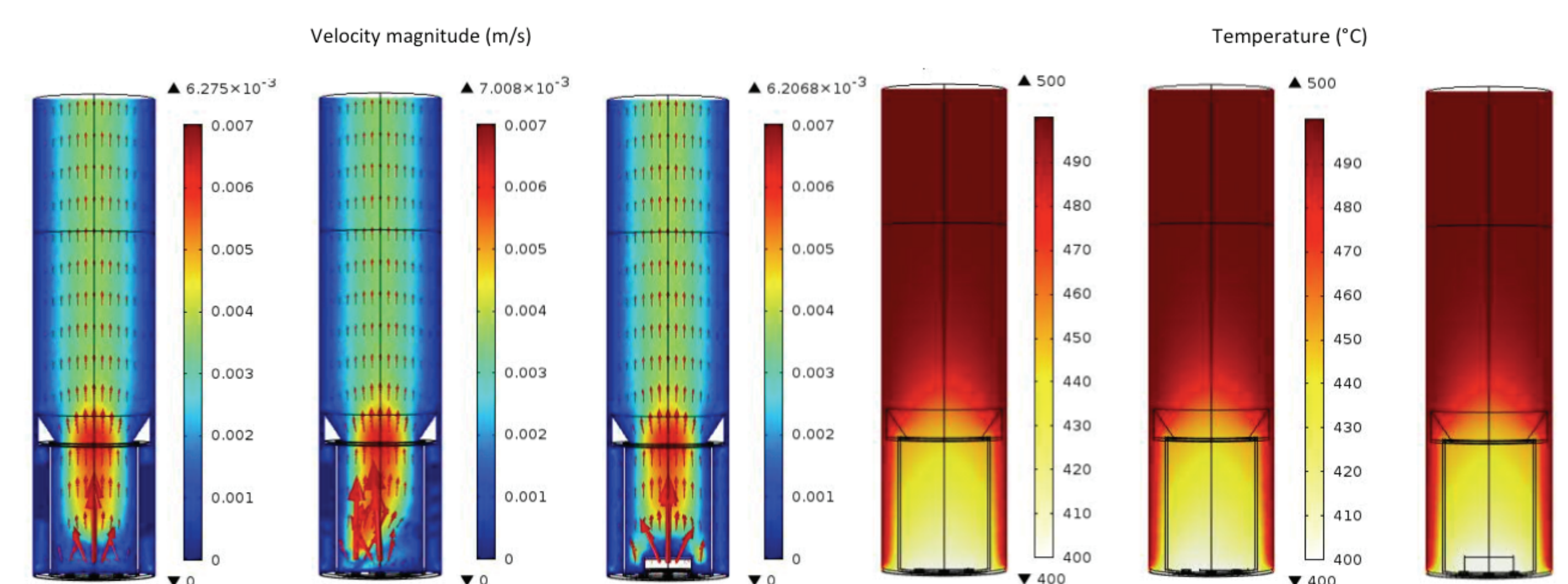


Figure 5. Effects of the introduction of composites

Conclusions

- The 3D COMSOL model is a useful tool for gaining a better insight into temperature and velocity profiles in the furnace during the steam-thermolysis;
- The increase of the steam flow rate and/or the furnace temperature leads a reduction in the residence time within the reactor. Conversely, the flow changes may affect the temperature profile within the crucible;
- The decomposition reaction of the composite polymer resin will be further integrated in the model.