CFD Investigation of Cross Bubbly Flow through a Column with Rectangular Geometry

N. M. Musa, D. Kuvshinov, P. Rubini

Chemical Engineering, School of Engineering and Computer Science, University of Hull, Hull, UK

Introduction:

Bubbly column reactors are multiphase reactors in which disperse phase (gas) is distributed into continuous phase by means of bubble diffuser (sparger). Co-current and counter-current flow bubble columns are widely applied in industry. A cross-flow is the more complicated case and has significant practical interest but less developed. Figure 1 and 2 presents advantages and challenges of using bubble column reactors.

Results:

Velocity profile is not symmetrical throughout the column and varies in magnitude Fig. 3. The velocity profile indicates that there is an intensive liquid circulation (vortex) developing in the column due to cross-flow.



Figure 1. advantages from bubble column

Computational Methods:

The model described laminar cross bubbly



Figure 3. gas and liquid velocity magnitude



flow in column with rectangular geometry. The laminar bubbly flow interface was used to simulate hydrodynamics parameters such as volume fraction of gas, gas and liquid velocity magnitude, flow regimes and liquid holdup in column.

Laminar bubbly flow continuity equation $\frac{\partial}{\partial x}(\rho_l\phi_l + \rho_g\phi_g) + \nabla (\rho_l\phi_lu_l + \rho_g\phi_gu_g) =$



Boundary	Materials	Туре	Value
Liquid inlet	30 wt % MEA	Volumetric flow rate	0.1-0.2 L/min
Gas inlet	Flue Gas	Volumetric flow rate	1-20 L/min
Liquid outlet	Rich-MEA	0 Pa	
Gas outlet	Gas outlet Treated Gas		

Figure 2. challenges

from bubble column

Table 1. Other boundary conditions

		Flue gas		Liquid Solvent	
Flux	L/min	1-20		0.1 – 0.2	
Mass content	%	N ₂	87.1	H ₂ O	70
		CO ₂	11.4	MEA	30
		H ₂ O	1.5	additives	0

Figure 5. Gas holdup vs superficial vel. For column without internal design



Figure 6. Gas holdup vs superficial velocity For column with internal design

Conclusions:

Hydrodynamics in bubble column varies significantly with change in internal design and configuration. Gas holdup depends on gas and liquid superficial velocity depending on internal design as presented on Fig. 5 & 6.

Table 2. Liquid and gas media composition

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1. Abd Ali M CFD simulation of bubbly flow through a bubble column. Int J Sci Eng Res 2014;5:7.

2. Tabib MV, Roy SA, Joshi JB CFD simulation of bubble column—an analysis of interphase forces and turbulence models. Chem Eng J 2008;139:589-614.

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